

1 **ACCEPTED PAPER (may differ slightly from the published copy)**

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3 **The removal of lead, copper, zinc and cadmium from aqueous solution by biochar**
4 **and amended biochars**

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16

Abstract

17 The exponential growth in the use of motor vehicles is a key contributor to freshwater

18 degradation. Current remediation techniques require prohibitively expensive

19 contaminant treatment and extraction. Biochar represents an inexpensive option to

20 ameliorate contaminants from motorway runoff. Biochar from Norway spruce (*Picea*

21 *abies* (L.) Karst.) was produced under fast pyrolysis-gasification (450–500 °C for 90 s)

22 and amended with wood ash and basaltic rock dust to evaluate sorption of Pb, Cu, Zn

23 and Cd. The column study, designed to mimic field conditions, confirmed that

24 unamended biochar can bind contaminants for short periods, but that the addition of

25 amendments, particularly wood ash, significantly improves contaminant removal.

26 Wood ash-amended biochar removed 98–100% of all contaminants during the study,
27 driven by pH ($r = 0.73\text{--}0.74$; $p < 0.01$ dependent on metal species) and phosphorus
28 levels causing precipitation ($r = 0.47\text{--}0.59$; $p < 0.01$, dependent on metal species). The
29 contaminants' progression through the biochar subsections in the column indicated that
30 increasing the thickness of the biochar layer increased contaminant residence time and
31 removal.

32 **Keywords – Biochar, Heavy metal, Highway runoff, Contaminant removal**

33

34 **Acknowledgements**

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36 (Swansea University), Dr. Ian Mabbett (Swansea University), Richard Haine (Frog
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38 (TerrAffix Soil Solutions)

39

Introduction

40
41 Motor vehicles are recognised as a growing source of pollution in modern society. As
42 of April 2018, there were c.38M licensed vehicles on Britain's roads, a number that has
43 been growing by c.640 thousand vehicles per year since 2012 (Gov.uk [2018](#)). Traffic
44 density is intrinsically linked to heavy metal contaminants (Hares and Ward [1999](#);
45 Ewen et al. [2009](#); Du et al. [2018](#)) and as such the exponential growth of motor vehicles
46 and resultant increases in traffic density has led to escalating amounts of pollution.
47 The growth in the number of motor vehicles naturally increases in conjunction with
48 highway development, increasing pollution and runoff volume. Development has
49 replaced significant areas of natural permeable land with artificial impermeable
50 surfaces (Ladislas et al. [2015](#)). These surfaces obstruct infiltration of precipitation into
51 the ground, increasing surface runoff, which washes away the polluted dust particles
52 resultant from anthropogenic activity (Ladislas et al. [2015](#); Charters et al. [2016](#);
53 Mohanty et al. [2018](#)).

54 Heavy metal motorway pollution is seen as a key contributor to freshwater degradation,
55 contaminating the food chain and enabling direct human exposure to toxins through
56 freshwater leisure activities. Numerous studies indicate that the impact of increased
57 metal concentrations on aquatic life is significant and can increase vulnerability to
58 disease, mortality and a reduction in fecundity (Burrows and Whitton [1983](#); Mayer-
59 Pinto et al. [2010](#); Yi et al. [2011](#); Wu et al. [2016](#)). Metal pollutants, such as Pb, Cu, Zn
60 and Cd, accrue in the aquatic environment, increasing their impact on aquatic species
61 and entering the food chain, causing increased concern globally (Cooper et al. [2009](#);
62 Wik et al. [2009](#); Kayhanian [2012](#)). Human exposure to these heavy metals can have
63 significant detrimental health consequences including the impairment of neurological
64 functions, kidney damage, liver function, fragile bones, lung damage and mortality

65 (Järup [2003](#); Ewen et al. [2009](#)).

66 Three key processes are currently used to remove pollutants: sedimentation, separation
67 and vegetated treatment processes. Current remediation techniques to remove heavy
68 metals from motorway runoff predominantly revolve around sedimentation, the
69 accumulation of which requires expensive treatment and extraction. For heavy metals,
70 capturing polluted sediment is the dominant method used through techniques such as
71 sedimentation tanks, balancing ponds (both wet and dry) and full retention oil traps.
72 Studies have shown heavy metal removal rates of these methods to be up to 70%
73 (Crabtree et al. [2006](#)). Whilst these methods reduce aqueous heavy metal
74 concentrations, over time polluted sediment builds up in the relevant tanks, traps and
75 ponds creating a toxic waste product that is difficult and costly to remove.

76 The dredging of toxic sediment in order to extract it from ponds is exceptionally
77 expensive (Rulkens [2005](#)). Depths of balancing ponds can be as shallow as 800 mm
78 with sediment accrual of up to 50 mm year⁻¹ such build up reduces the removal
79 efficiency of ponds, putting nearby waterbodies at risk whilst exposing wildlife to
80 toxins within the ponds (Farm [2002](#); Karlsson et al. [2010](#); Weinstein et al. [2010](#)).

81 Biochar deployment is a potential alternative to current processes commonly used to
82 remove pollutants. Biochar is the carbon rich porous product produced by pyrolysis
83 from plant- and animal-based biomass under oxygen limited conditions, with an
84 appearance similar to charcoal (Lehmann and Joseph [2009](#)). It can be produced using a
85 multitude of feedstocks and a variety of pyrolysis conditions, both of which are key to
86 controlling its properties (Xiao et al. [2018](#)).

87 Biochar can be used to remove heavy metal contaminants from polluted water
88 principally as a result of its sorption properties (Kilic et al. [2013](#)). Immobilisation of
89 heavy metals takes place through several mechanisms including ionic bonding, cation

90 exchange, physical adsorption and co-precipitation (Zhang et al. [2013](#); Wang et al.
91 [2018](#)).

92 The efficacy of the immobilisation is influenced by the characteristics of three key
93 factors:

94 **The biochar**

95 Biochar characteristics differ with feedstock and pyrolysis conditions. These
96 differences influence bulk physical properties such as surface area and porosity (Mohan
97 et al. [2007](#); Ifthikar et al. [2017](#)) and chemical properties such as functional groups,
98 mineral ash and pH which are instrumental in the binding of heavy metals to biochar
99 (Uchimiya et al. [2010](#); Xu et al. [2013a](#); Lehmann and Joseph [2015](#)). Surface area and
100 total pore volume are intrinsically linked as highly porous structures, particularly
101 micropore structures, have a high surface area (Chen et al. [2011](#); Mohan et al. [2014](#)). It
102 has been noted that surface area and porosity facilitate the adsorption of heavy metals
103 as a result of the volume of potential adsorption sites and that these physical properties
104 are controlled partly by pyrolysis conditions but to a greater extent by feedstock (Chen
105 et al. [2011](#)). Oxygenated functional groups are a critical chemical property which act as
106 a key factor contributing to heavy metal adsorption as a result of electrostatic attraction
107 (Wang et al. [2018](#)) with relevant groups such as carboxyl being present in biochar at
108 high pH values (Bogusz et al. [2015](#)). pH also impacts precipitation with higher biochar
109 pH values enabling precipitation of Pb, Cu, Zn and Cd by carbonate and phosphate
110 minerals (Inyang et al. [2012](#)). Elemental composition, for instance alkali metal and
111 alkaline earth concentrations, can also be changed via feedstock and pyrolysis
112 conditions, affecting biochar pH and cation exchange capacity (CEC) (Zhang et al.
113 [2013](#)). Additionally, carbon structure, a key driver of complex bonding, can be
114 manipulated through pyrolysis conditions such as temperature (Schreiter et al. [2018](#)).

115 **The medium**

116 The characteristics of the containing medium such as soil, sediment or aqueous solution
117 (for example motorway runoff) also impact immobilisation. Relevant characteristics
118 here include the pH and temperature of the medium, concentrations and quantities of
119 the contaminant and organic matter abundance. The pH of the medium is key to the
120 surface charge of the biochar and therefore electrostatic interactions; with increasing
121 pH, there is an increasing negative charge due to deprotonation of acidic functional
122 groups (Wang et al. [2018](#)). The pH of the medium can also influence heavy metal
123 speciation, which is instrumental in immobilisation (Kilic et al. [2013](#); Trakal et al.
124 [2014](#)). Increasing the temperature of the medium increases adsorption, as heavy metal
125 ions are provided with enough energy to reach and adsorb onto biochar's interior
126 structure (Liu and Zhang [2009](#)).

127 **The contaminant**

128 Finally, the characteristics of the contaminant also play a role in immobilisation. The
129 efficacy of biochar's remediation of heavy metals shows strong dependency on
130 contaminant type (Inyang et al. [2012](#)). Due to the importance of ionic bonding in the
131 adsorption process, the stronger the positive valence on the metal ions, the greater the
132 potential for adsorption (Kilic et al. [2013](#)). The ionic radius is also of importance, with
133 smaller radii being more easily adsorbed (Ko et al. [2004](#)). The role that the contaminant
134 plays in adsorption is indicated by the fact that different contaminants are more readily
135 adsorbed by different types of biochar (Lehmann and Joseph [2009](#)).

136 These well-understood sorption mechanisms are often explored in batch or continuous
137 flow column studies which provide results unlikely to be reproduced in the field. Batch
138 studies produce a laboratory-based maximum sorption capacity to quantify contaminant
139 removal where potential removal is recorded. Although a closer approximation to field

140 conditions than batch studies, continuous flow column studies are also still specifically
141 designed to preclude issues encountered in the field such as channelling effects and
142 clogging, again resulting in removal values difficult to achieve in the field (Ramírez-
143 Pérez et al. [2013](#); Callery et al. [2016](#); Arán et al. [2017](#)).
144 This pulse column study moves further away from maximum sorption capacity and
145 towards complex field approximation where issues such as preferential flow and
146 sporadic precipitation are recreated. The primary aim of this study is to ascertain the
147 efficacy of biochar and amended biochars as an affordable remediator for heavy metals
148 from motorway runoff, specifically Pb, Cu, Zn and Cd. The study focused on heavy
149 metal pollutants due to their toxicity, non-biodegradable nature and bioavailability in
150 receiving waterbodies. The depth of immobilisation and retention times of biochar and
151 amended biochars were investigated to assess the potential for the approach to be
152 scaled-up and used in the field.

153

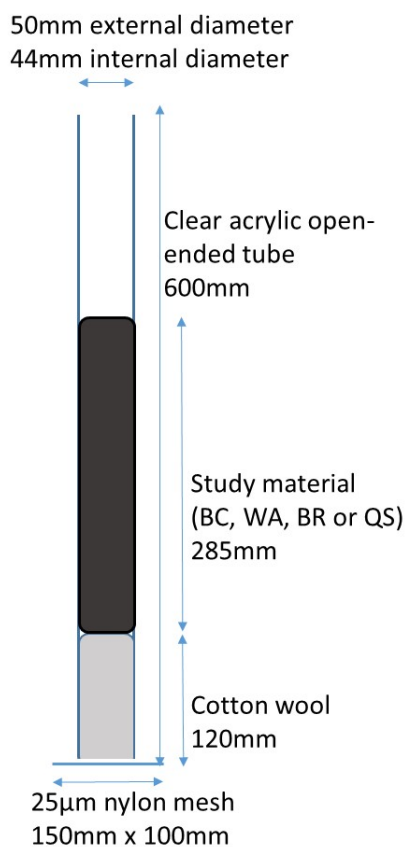
154 **Methods and materials**

155 **Pilot study**

156 Preliminary work was undertaken to determine the residency time of a solution within a
157 biochar water column; residency being intrinsically linked with the potential for
158 sorption (Mohanty et al. [2018](#)). Four water columns were established containing 50 g,
159 80 g, 90 g and 100 g of biochar, respectively, to determine the appropriate volume of
160 biochar to be used during the main study. Each volume was held in a clear, acrylic,
161 open-ended tube, with a column height of 600 mm, an interior diameter of 44 mm and a
162 3-mm thick wall (Fig. [1](#)). Each acrylic tube was held in place at 300 mm above bench
163 level with a clamp stand, enabling a 1-L bottle with a funnel lined with a Whatman 11-
164 μm qualitative filter paper to be situated underneath to capture the eluate. A 25- μm

165 nylon mesh (150 mm × 100 mm) was attached to the base of each water column to
166 prevent the loss of biochar. Between the base of the biochar and the nylon mesh,
167 120 mm of cotton wool was inserted to allow any eluate to drain away whilst reducing
168 re-contact with the study material. Water columns were kept at room temperature and
169 covered with filter paper to reduce evaporation. The quantity (mL) and retention time
170 (min) of the solution were all measured for each volume of biochar.

171



172

173 **Fig 1.** Water columns into which the aqueous solution was administered for biochar (BC), biochar
174 amended with wood ash (WA), biochar amended with basaltic rock dust (BR) and quartz sand (QS).

175

176 **Selection and preparation of biochar, amendments and control**

177 The biochar used in this study consisted of Norway spruce (*Picea abies* (L.) Karst.)

178 wood chips pyrolyzed in a Pyrocal BigChar-1000 pyrolysis-gasification kiln at a

179 temperature of 450–500 °C, with a retention time of ~ 90 s and was granulated
180 (< 3 mm). Norway spruce, as a softwood, was chosen because of its greater number of
181 pores and surface area for sorption to take place in comparison with hardwood
182 (Mohanty et al. [2018](#)). Amendments to the biochar were mixed dry at room
183 temperature, at a ratio of 1:1, with a plasterer's whisk. Mixed wood ash was selected as
184 an amendment due to its high pH, phosphorus (P) and alkaline earth content (Mg and
185 Ca). Basaltic rock dust was used because of its high pH and alkaline earth content (Mg
186 and Ca). Quartz sand was employed as a control due to its neutral pH, low levels of
187 alkaline earth and low levels of heavy metal pollutants.

188

189 **Pre-study analysis**

190 pH measurements were carried out by soaking biochars with deionised water at a 1:5
191 solid/water ratio for 24 h in a 150-mL Sterilin plastic screw top container, which was
192 agitated on a Unitwist 400 Orbital Shaker. The pH of the resultant slurry was measured
193 using a previously calibrated Voltcraft pH Meter that was rinsed with deionised water
194 between samples. The pH for the quartz sand control was determined by adding 50 g of
195 sand to 100 mL of deionised water in a 150-mL Sterilin plastic screw top container
196 which was agitated for 1 h before measuring the pH. The elemental composition of the
197 biochar, amended biochars and quartz sand was determined using a benchtop Rigaku
198 NEX CG Energy-Dispersive XRF spectrometer, which was calibrated with internal
199 standards. He, rather than air, was used in the XRF chamber to ascertain heavy metal
200 (Pb, Cu, Zn and Cd), alkali metal (K), alkaline earth (Mg and Ca) and P concentrations.
201 Samples of each of the study materials were dried at 50 °C for 24 h and ground using a
202 pestle and mortar to minimise gaps between sample particles within XRF sample
203 containers, reducing air pockets and giving more precise analytical results. These

204 samples were transferred, in triplicate, into Scimed polyethylene sample cups of 32-
205 mm diameter using 4- μ m Prolene films for support. The containers were filled between
206 5 and 10 mm with the samples which were then pressed manually further reducing air
207 pockets, the sample mass determined and placed in the XRF spectrometer. Samples
208 were analysed in batches of 15 and results were calculated as concentration values (in
209 mg L⁻¹) before conversion to percentage change from solution. Each sample was
210 analysed in triplicate to determine XRF precision and the mean value used in further
211 calculations.

212

213 **Water column experiment**

214 To evaluate the efficacy of biochar's immobilisation of Pb, Cu, Zn and Cd, a study
215 using aqueous solutions was undertaken. The study consisted of four sets of four
216 replicate water columns with set 1 containing biochar (BC), set 2 containing biochar
217 amended with wood ash (WA), set 3 containing biochar amended with basaltic rock
218 dust (BR) and set 4 containing the quartz sand control (QS). The water column set up
219 used in the pilot study was repeated for the full study (Fig. 1). As a result of the pre-
220 trial residence test, 90 g of biochar was added to each of the first set of four replicate
221 water columns and compressed with an aluminium rod to a height of 285 mm with a
222 volume of ~ 450 mL. This volume was then used as a template for the sets of water
223 columns holding WA, BR and QS.

224

225 **Heavy metal solution**

226 Liu and Zhang (2009) studied biochar's sorption of Pb in aqueous solution up to a
227 concentration of up to 40 mg L⁻¹. Hence, a solution containing 40 mg L⁻¹ of each
228 contaminant (Pb, Cu, Cd and Zn) was used in this study to stress the biochars beyond

229 what would be encountered in field conditions (Crabtree et al. [2009](#); Zhao et al. [2010](#);
230 MacKay et al. [2011](#)). The stock solution was mixed in a grade A volumetric flask
231 (5000 ± 1.2 mL) within a fume cabinet. Deionised water was added to half fill the
232 volumetric flask. Two hundred millilitres of each of the four single element Fisher
233 1000 mg kg⁻¹ heavy metals of AAS standard grade was added using a 50-mL glass
234 pipette. The metal standards were held in 5% HNO₃ and as such the study eluent
235 constituted an acidic solution whereby all four metals were dissolved. Forty-two
236 millilitres of this solution was added to each column at 24-h intervals via a syringe.
237 This volume was calculated from an average of the highest 30 daily precipitation values
238 in South East England during the period 2000 to 2018, to mimic both severe first
239 flushing after an antecedent dry period and the sporadic nature of precipitation in the
240 field (Metoffice.gov.uk [2018](#)). Eluate samples were collected every 6 days, allowing
241 24 h after the day six solution was added, for the duration of the study.

242

243 **Eluate analysis**

244 Analysis of the eluate was conducted by XRF to determine heavy metal (Pb, Cu, Cd
245 and Zn), alkali metal (K), alkaline earth (Mg and Ca) and P concentrations. Fifty
246 millilitres of 6-day eluate from each water column and from the solution batch was
247 stored in 50-mL centrifuge tubes at room temperature. XRF cannot directly measure
248 liquids as they would evaporate in the vacuum chamber (P. Brouwer, pers. comm.,
249 [2010](#)). As a result, Rigaku Ultra Carry Light disks were used for the analysis of the
250 eluate, which enabled the concentrations (in mg L⁻¹) to be determined for Pb, Cu, Zn,
251 Cd, Mg, Ca, K and P. Two hundred microlitres of eluate was pipetted onto the filter
252 paper portion of the Ultra Carry Light disk for each sample. Each disk was left to dry
253 for 8 h at room temperature prior to analysis. The XRF chamber was evacuated and the

254 eluate on the disks was analysed in batches of 15 samples in triplicate.

255

256 **Subsection analysis**

257 Post-day 36, each water column was frozen at $-20\text{ }^{\circ}\text{C}$ for 24 h to enable each column

258 to be cut into five equal subsections. Whilst freezing has been found to change metal

259 speciation, it does not change total metal concentration (Florence [1977](#); Batley [1990](#)).

260 Analysis of each subsection was undertaken by XRF, using He in the chamber to

261 determine heavy metal concentrations (Pb, Cu, Zn and Cd). As detection of elements

262 by XRF is affected by water content (Roberts [2015](#)), solid samples were dried for 24 h

263 at $50\text{ }^{\circ}\text{C}$ before XRF analysis. The proportion of contaminant held in each subsection

264 was then determined to understand the movement of contaminant through the study

265 material in each water column.

266

267 **Statistical analysis**

268 Comparisons between the different biochars' contaminant removal values were

269 performed using the Kruskal-Wallis test using a probability threshold of $p = 0.01$.

270 Correlation analysis using Pearson's R was undertaken to test relationships between

271 heavy metal remediation and biochar characteristics.

272

273 **Results**

274 **Pre-study contaminant concentrations**

275 For the biochar and amended biochars the levels of intrinsic contaminant metals were

276 low (Table 1).

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Study Materials	Pre-study contaminant concentration			
	Cd (mg.kg ⁻¹)	Cu (mg.kg ⁻¹)	Pb (mg.kg ⁻¹)	Zn (mg.kg ⁻¹)
Biochar (BC) average	0 ± 0	12 ± 0	7 ± 0	48 ± 1
Biochar amended with wood ash (WA) average	0 ± 0	134 ± 2	79 ± 1	371 ± 8
Biochar with basaltic rock dust (BR) average	0 ± 0	24 ± 1	18 ± 0	81 ± 2
Quartz sand (QS) average	0 ± 0	8 ± 0	0 ± 0	4 ± 0

284 **Table 1.** Pre study concentration of heavy metal contaminants in biochar, amended biochar and quartz
285 sand (mg.kg⁻¹)

286

287 **Pre-study P, pH, Mg, K and Ca measurements**

288 P, pH, Mg, K and Ca were quantified for each study material in pre-study analysis
289 (Table 2). For each of these five categories, WA displayed the highest pre-study levels.
290 BR had the second highest levels in terms of pH, Mg, Ca and K. BC was third in most
291 categories with the exception of P where it displayed low concentrations in comparison
292 with WA rather than the undetectable amounts of P in BR and QS. QS, as the control,
293 displayed the lowest values of all of the properties measured.

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	Pre-study levels of pH and alkali and alkaline earth				
Study materials	pH	P (mg.kg ⁻¹)	Mg (mg.kg ⁻¹)	K (mg.kg ⁻¹)	Ca (mg.kg ⁻¹)
Biochar (BC) average	8.7 ± 0.0	35 ± 11	0 ± 0	4040 ± 139	8080 ± 197
Biochar amended with wood ash (WA) average	11.5 ± 0.0	4770 ± 108	16700 ± 578	35700 ± 788	208000 ± 5030
Biochar with basaltic rock dust (BR) average	10.2 ± 0.0	0 ± 0	13900 ± 521	9850 ± 38	35200 ± 38
Quartz sand (QS) average	7.5 ± 0.0	0 ± 0	0 ± 0	542 ± 18	112 ± 8

301

302 **Table 2.** Pre study levels of pH, P, alkali and alkaline earth in biochar, amended biochar and quartz sand

303

304 **Eluate and subsection analysis:**

305 ***Pb eluate***

306 Pb was the contaminant most successfully remediated by the biochar and amended

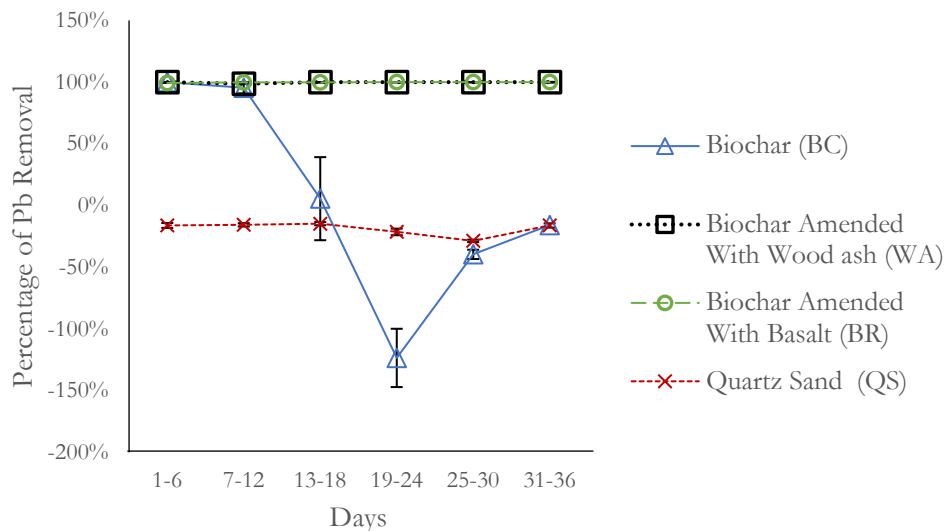
307 biochars. Elimination rates for BC, WA and BR started at 99–100% (Fig. 2). By days

308 13–18, BC started to show reduced removal of contaminants and by days 19–24, it had

309 started to desorb, adding Pb to the eluate. Desorption decreased until days 31–36 when

310 remediation levels matched QS control levels. WA and BR maintained elimination

311 rates of 99–100% for the remainder of the study. QS, as the control, did not decrease
 312 Pb concentration. Over the duration of the study, WA and BR removed 100% of Pb
 313 showing no significant difference in efficacy between them, whereas BC only removed
 314 4%, significantly less than both WA and BR, with QS at – 19%.
 315

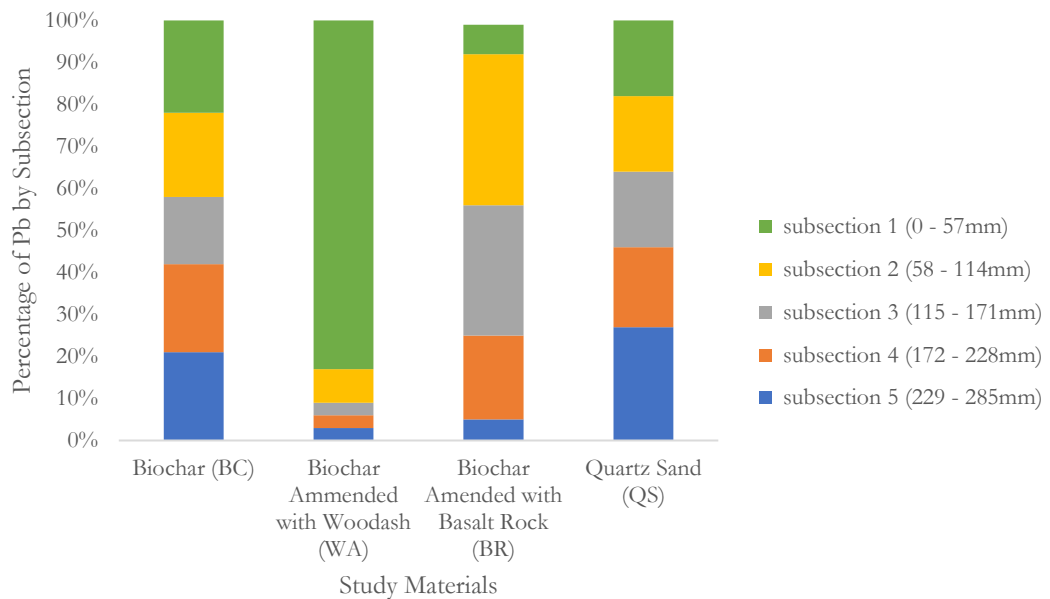


316
 317 **Fig 2.** The removal and desorption of lead in percentage terms for each of the study materials over the
 318 duration of the study. Values below quartz sand control levels represent desorption.

319
 320 ***Pb distribution in the column subsections***

321 The proportions of Pb at each 57-mm subsection varied between the study materials
 322 (Fig. 3). BC, which desorbed Pb and returned to control levels of remediation by the
 323 end of the study (Fig. 2), showed no significant difference between the concentrations
 324 of Pb in each subsection and showed no significant differences from the subsections of
 325 the QS control. WA, which immobilised 100% of Pb (Fig. 2), held 83% of the
 326 contaminant in the first subsection with only 3% in the final subsection (Fig. 3). BR,
 327 which also removed 100% of Pb (Fig. 2), showed a far smaller percentage than WA in
 328 the first subsection (5%), with 87% of Pb held in subsections 2, 3 and 4, with only 7%

329 held in subsection 5 (Fig. 3). These proportions indicate that as the study material
 330 reached maximum removal capacity, Pb moved through the subsections until, post-
 331 desorption, proportions of the contaminant were lessened and became equal throughout
 332 the layers.
 333



334
 335 **Figure 3.** The relative proportion of lead in each 57mm subsection for each study material post study.
 336

337 ***Cu eluate***

338 Cu elimination rates for BC, WA and BR were found to be 99–100% during days 1–6
 339 (Fig. 4). BC elimination rates declined on days 7–12 and continued to drop until
 340 desorption reached its maximum on days 19–24. Removal by BC had returned to
 341 control levels by days 31–36. BR maintained its initial Cu removal percentage until
 342 days 31–36 when capacity was reached and desorption began (Fig. 4). WA maintained
 343 elimination rates of 98–100% for the entirety of the study. In contrast, QS, as the
 344 control, did not decrease the Cu concentration. Over the duration of the study, WA
 345 removed 99% of Cu, significantly more than the other three materials; in contrast, BR

346 removed 74%, significantly higher than BC, which removed 1% with QS at -19%.

347 at -19%.

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358 **Figure 4.** The removal and desorption of copper in percentage terms for each of the study materials over
359 the duration of the study. Values below quartz sand control levels represent desorption.

360

361 *Cu distribution in the column subsections*

362 BC desorbed Cu (Fig. 4) and displayed no significant difference in Cu concentrations

363 between subsections. Similarly, QS which did not remediate Cu showed no significant

364 difference in proportions of Cu between each subsection. WA removed Cu at 99%,

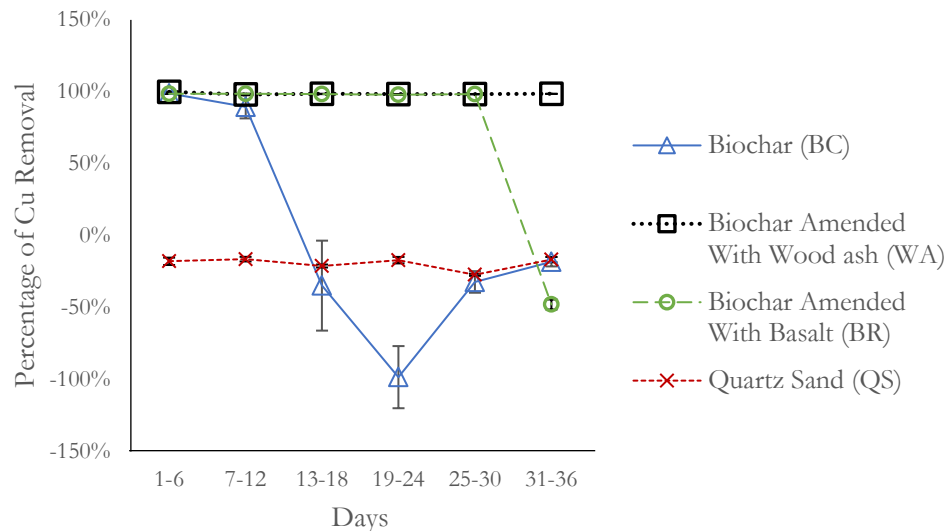
365 (Fig. 4) holding 80% in subsection 1 (Fig. 5) with only 4% in the final subsection. BR

366 showed signs of desorbing Cu on days 31–36, reflected by 30% of Cu being held in the

367 final subsection. These proportions suggested that the contaminant was in the process

368 of draining out of the water column due to desorption.

369



356

357

358 **Figure 4.** The removal and desorption of copper in percentage terms for each of the study materials over
359 the duration of the study. Values below quartz sand control levels represent desorption.

360

361 *Cu distribution in the column subsections*

362 BC desorbed Cu (Fig. 4) and displayed no significant difference in Cu concentrations

363 between subsections. Similarly, QS which did not remediate Cu showed no significant

364 difference in proportions of Cu between each subsection. WA removed Cu at 99%,

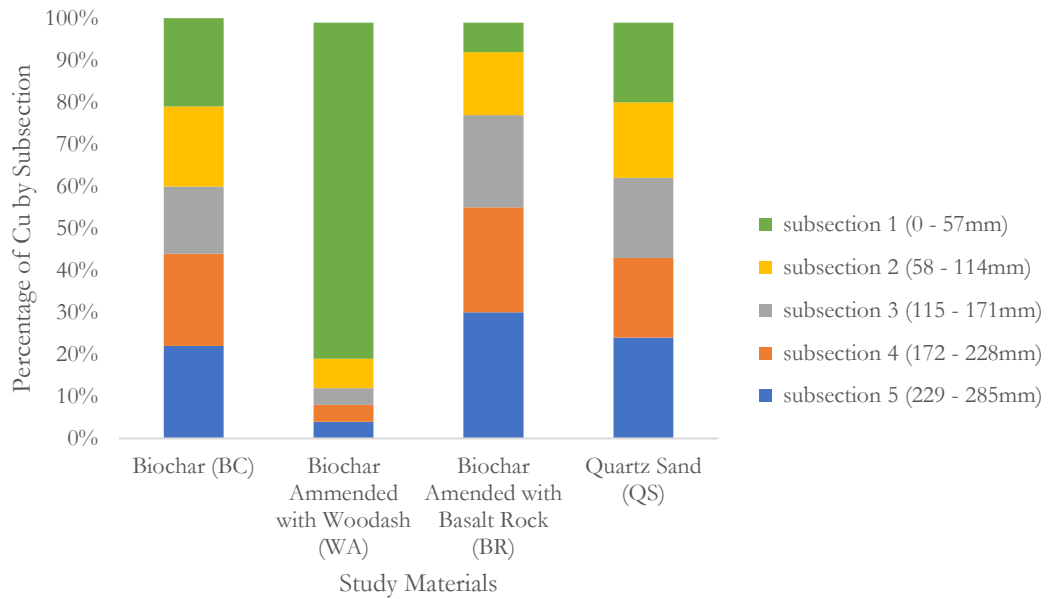
365 (Fig. 4) holding 80% in subsection 1 (Fig. 5) with only 4% in the final subsection. BR

366 showed signs of desorbing Cu on days 31–36, reflected by 30% of Cu being held in the

367 final subsection. These proportions suggested that the contaminant was in the process

368 of draining out of the water column due to desorption.

369



370

371 **Figure 5.** The relative proportion of copper in each 57mm subsection for each study material post study.

372

373 ***Zn eluate***

374 Zn elimination rates for BC, WA and BR started at 98–100%. BC removal rates started
 375 to decline by days 7–12 with a drop to 84% (Fig. 6). By days 13–18, it had begun to
 376 desorb and continued to do so during days 19–24. Remediation returned to near control
 377 levels by days 25–30 and was at control levels by days 31–36. BR maintained 98% Zn
 378 removal until days 19–24 when elimination rates dropped to 67% where they stayed for
 379 days 25–30. However, desorption took place by days 31–36. WA removal of Zn
 380 remained between 97 and 100% for the period of the study. Again, QS, as the control,
 381 did not decrease the Zn concentration. Over the duration of the study, WA removed
 382 98% of Zn, again demonstrating significantly higher removal than all other study
 383 materials, BR removed 52%, which was significantly higher than BC, which removed
 384 – 11% with QS at – 21%.

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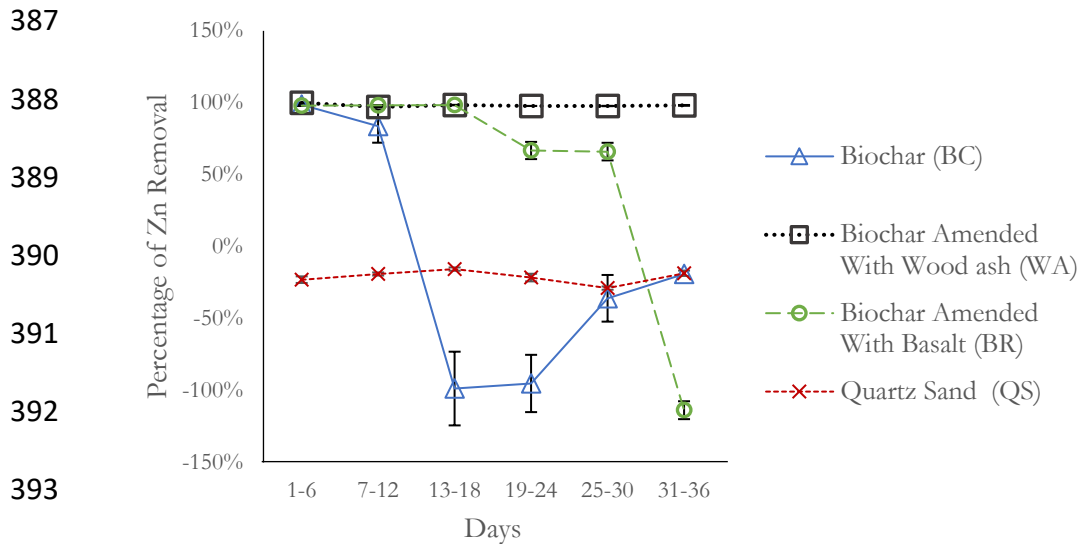
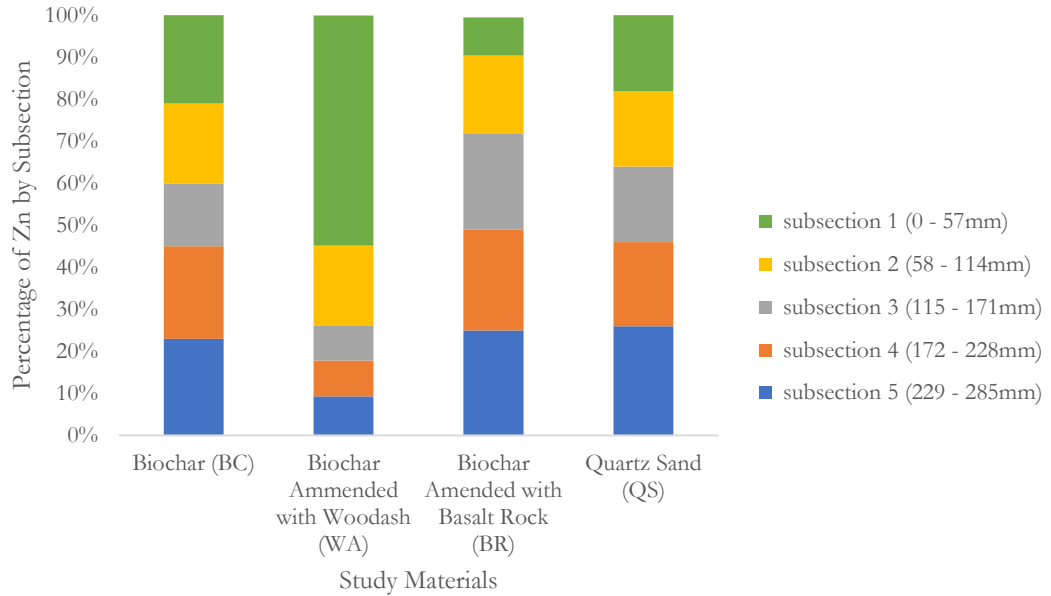


Figure 6. The removal and desorption of zinc in percentage terms for each of the study materials over the 36 day duration of the study. Values below quartz sand control levels represent desorption.

Zn distribution in the column subsections

Again, BC and the QS control showed no total net removal for Zn (Fig. 6) and as such Zn proportions showed no significant difference between the 57-mm subsections (Fig. 7). BR showed only 9% of Zn held in subsection 1, with the largest proportion seen in subsection 5 (25%). This signified that Zn was leaving the study material, as demonstrated by BR's desorption of Zn on days 31–36. Although WA did not desorb Zn during the trials, there is evidence that the contaminant was moving down the subsections with only 55% retained in subsection 1 and 19% in subsection 2 (Fig. 7).



407

408 **Figure 7.** The relative proportion of zinc in each 57mm subsection for each study material post study.

409

410 ***Cd eluate***

411 Overall Cd was the contaminant that was least successfully removed. Removal by BC,
 412 WA and BR was at 100% for days 1–6 (Fig. 8). However, BC elimination rates of Cd
 413 started to decline by days 7–12. Desorption was seen by days 13–18 and continued into
 414 days 19–24 before returning to control levels by days 25–30 where it remained for days
 415 31–36. BR maintained 100% of Cd removal until days 19–24 when a marked drop
 416 occurred to just above control levels (Fig. 8). Control levels were reached pre-
 417 desorption during days 25–30 but desorption occurred on days 31–36. However, WA
 418 maintained Cd elimination rates of 100% throughout the study. Again QS, as the
 419 control, did not decrease the Cd concentration of the eluate. Whilst Cd proved to be the
 420 contaminant that was least successfully immobilised amongst biochar and amended
 421 biochars overall (Fig. 8), WA still removed 100% of Cd, significantly more than BR, at
 422 29%, which in turn was significantly higher than BC, at 5% removal, with QS at
 423 – 20%.

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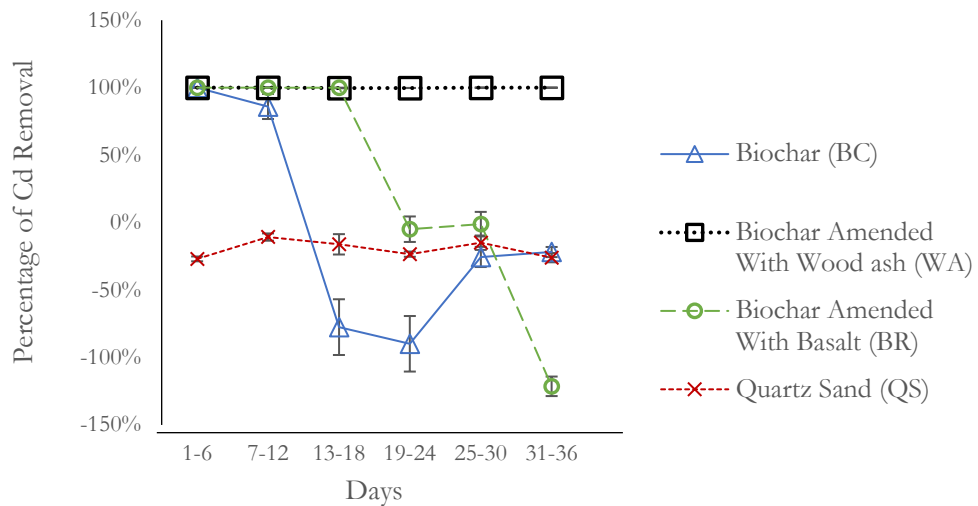
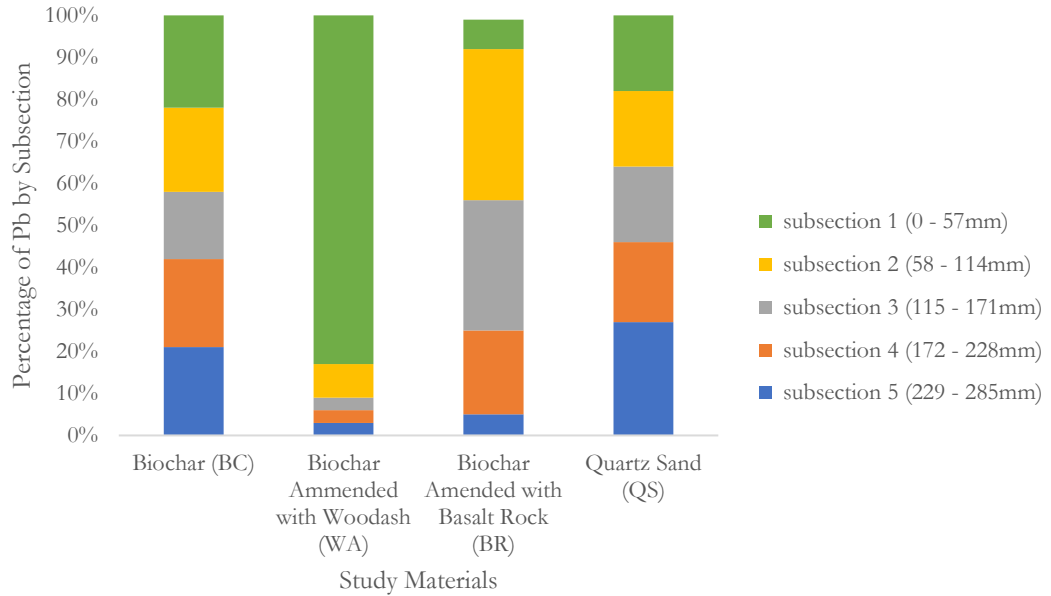


Figure 8. The removal and desorption of zinc in percentage terms for each of the study materials over the 36 day duration of the study. Values below quartz sand control levels represent desorption.

Cd distribution in the column subsections

BC and QS both showed a relatively even distribution of Cd between the 57-mm subsections (Fig. 9), indicative of their lack of total net Cd removal (Fig. 8). Although BR removed more Cd than BC and QS over the first 30 days, it had started to desorb all three contaminants by days 31–36, a process reflected in the proportions of contaminant held in the subsections. Cd proportions in each WA subsection (Fig. 9) were concentrated in subsection 1, as removal was still taking place.



445

446 **Figure 9.** The relative proportion of cadmium in each 57mm subsection for each study material post
 447 study.

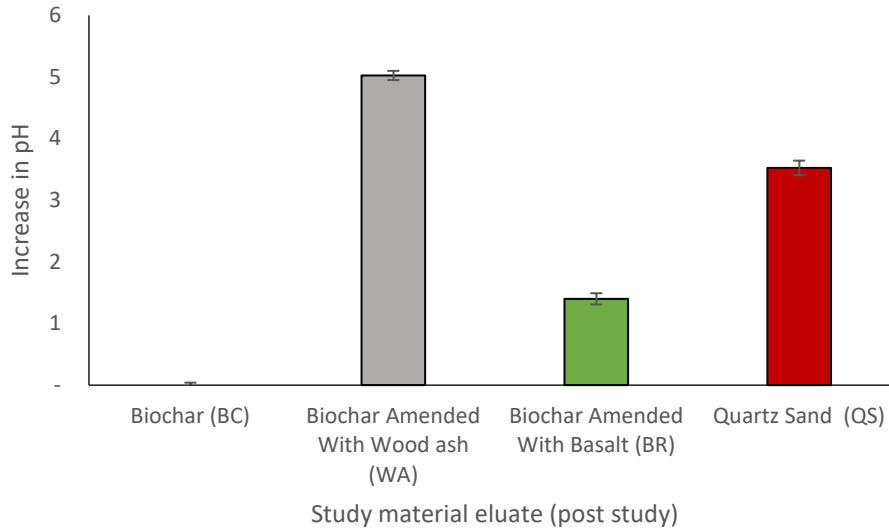
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449 ***Eluate pH***

450 The pH increase from eluent to eluate showed significant differences between study
 451 materials (Fig. [10](#)). WA caused the highest eluate pH change, BR the second and BC
 452 the lowest. BC, WA and BR neutralised the acid eluent to varying degrees during the
 453 study, in line with the concentrations of alkali and alkaline earths seen in each study
 454 material (Table [2](#)). Correlations between contaminant removal and eluate pH were
 455 $r = 0.73-0.74$; $p < 0.01$ (dependent on metal).

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459 **Figure 10.** The change in pH levels from eluent to eluate by study material

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Discussion

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In this study, we investigated the ability of biochar to remove heavy metal pollutants,

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specifically Pb, Cu, Zn and Cd, from motorway runoff. This remediation takes place

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due to the physical and chemical properties of the (amended)-biochar enabling the

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removal of these contaminants (Lu et al. [2012](#)). It was also hypothesised that biochar's

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removal efficacy of polluted motorway runoff can be improved through amendments,

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such as the addition of wood ash or basaltic rock dust. The study confirmed that

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biochar can immobilise contaminants for a short period but that the addition of

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amendments, particularly wood ash, significantly improves the ability to immobilise all

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contaminants examined in this study for an extended time period (Figs. [2](#), [4](#), [6](#) and [8](#)).

471

The principal factors affecting removal have been examined in relation to each metal

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for biochar (BC), biochar amended with wood ash (WA) and biochar amended with

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basaltic rock dust (BR), to ascertain their respective importance in the removal process

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for each contaminant studied. WA displayed the highest pre-study levels of pH, P, Mg,

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K and Ca, which were hypothesised to increase contaminant removal. WA also showed

476 the largest increase in pH from eluent to eluate partly as a result of the release of oxides
477 and carbonates in the ash causing alkalinity to increase (Cerrato et al. [2016](#)). Such
478 deprotonation likely increased the negative surface charge of the biochar increasing the
479 electrical attraction of the metal cations and changed the dissociation of surface
480 functional groups (Xiao et al. [2018](#)). Phosphorus minerals have also been seen to
481 contribute to the sorption of Pb, Cu, Cd and Zn through precipitation as insoluble
482 phosphate salts at higher pH (Lehmann and Joseph [2015](#)). Furthermore, the increased
483 pH also decreased the solubility of heavy metals in solution leading to their
484 precipitation (Pourbaix [1966](#)). The pre-study hypothesis that WA would be the most
485 successful remediator, with the greatest potential to be scaled up, was borne out during
486 the study (Figs. [2](#), [3](#), [4](#), [5](#), [6](#), [7](#), [8](#) and [9](#)).

487 **Pb sorption**

488 Several key factors influenced the sorption of Pb during this study. The principal factor
489 of importance was pH, which showed a strong correlation with Pb removal ($r = 0.73$;
490 $p < 0.01$) supporting the results of previous studies (Xu et al. [2013b](#); Mohan et al. [2007](#))
491 and Wang et al. [2018](#)). Mohan et al. ([2007](#)) asserted that the maximum absorption of Pb
492 occurred between pH 4 and 5, close to the post-study pH of the WA eluate, which
493 ranged from pH 5.4 to 5.8. pH changes Pb speciation at low pH, at which it is found in
494 soluble form (Pb²⁺) rather than the Pb precipitate Pb(OH)₂ found at higher pH
495 (Pourbaix [1966](#)). BC was not as successful in its removal of Pb (Fig. [2](#)) and showed pH
496 levels well below the maximum sorption range outlined in Mohan et al.'s ([2007](#)) study.
497 The concentration of total P in the eluate showed a strong negative correlation with
498 sorption of Pb ($r = -0.59$; $p < 0.01$). The higher the amount of P lost from the study
499 materials to the eluate, the lower the amount of P that was available within the study
500 materials to cause precipitation. Uchimiya et al. ([2010](#)) observed that the remediation

501 of Pb was primarily as a result of phosphate-based ligands forming Pb phosphate
502 precipitates. Cation exchange capacity (CEC) was also of importance to Pb remediation
503 in this study, through the exchange of Mg ($r = 0.50$; $p < 0.01$) and Ca ($r = 0.58$;
504 $p < 0.01$), as reported by Lu et al. (2012). However, contrary to published research (Lu
505 et al. 2012), K ion exchange was not of strong importance in this study ($r = 0.30$;
506 $p < 0.01$).

507 **Cu sorption**

508 As for Pb, the eluate pH value showed the most significant correlation with Cu sorption
509 ($r = 0.74$; $p < 0.01$). This is in line with Chen et al. (2011) who noted how pH
510 significantly affected the removal of both Cu and Zn. Removal levels were reported to
511 rise with pH levels until a pH of 5 was reached, agreeing with this study's finding.
512 With a pH value of < 4 , reduced available negative sorption sites due to competition
513 from H^+ ions and a soluble metal speciation (Cu^{2+}) will be found. This would go some
514 way towards explaining the significant differences between WA and BC in terms of
515 sorption of Cu (Figs. 4 and 5).

516 Eluate P levels (and therefore a reduction in study material P levels) showed a negative
517 correlation with Cu sorption ($r = -0.54$; $p < 0.01$). This is likely as a result of
518 precipitation with PO_4^{3-} (Xu et al. 2013b). Xu et al. (2013b) asserted that metal
519 phosphate and metal carbonate precipitation 75–100% of Cu sorption. Whilst this study
520 indicated that precipitation as a result of pH and P is the dominant factor in Cu
521 removal, contrary to Xu et al. (2013b), CEC has some limited relevance through the
522 exchange of Ca (Ca: $r = 0.53$, $p < 0.01$, Mg: $r = 0.29$, $p < 0.01$ and K: $r = 0.35$, $p < 0.01$).

523 **Zn sorption**

524 As for Pb and Cu, eluate pH displayed the strongest correlation with Zn sorption
525 ($r = 0.74$, $p < 0.01$) further supporting the conclusions of Chen et al. (2011) regarding

526 the significance of pH for the remediation of both Zn and Cu. Zn displays very similar
527 removal drivers to Cu with pH and P being the primary drivers and CEC having a
528 moderate or weak impact on sorption. Of the four study contaminants, the similarities
529 between Cu and Zn are not unexpected due to their similar electron structure and size
530 of ionic radius (Park et al. [2015](#)). Again, eluate P levels showed a strong negative
531 correlation with Zn sorption ($r = -0.54$; $p < 0.01$). As with Cu, Xu et al. ([2013b](#))
532 attributed Zn sorption to precipitation, citing PO_4^{3-} as an important factor. CEC was a
533 minor factor in sorption of Zn with moderate sorption correlation with Ca ($r = 0.42$;
534 $p < 0.01$) and K ($r = 0.35$; $p < 0.01$) and a weak or no correlation with Mg ($r = 0.16$;
535 $p < 0.13$). The moderate sorption correlation with Ca contradicts Xu et al. ([2013b](#)) who
536 observed no link to CEC but rather saw removal as entirely the result of precipitation.

537 **Cd sorption**

538 Cd was the contaminant least susceptible to removal across the study materials (Figs. [8](#)
539 and [9](#)). Despite this overall trend, Cd elimination rates by WA were at 100% and
540 showed no indications of desorption, even from the progression of Cd through the WA
541 subsections (Fig. [9](#)). Again, pH was the most influential factor in sorption ($r = 0.74$;
542 $p < 0.01$) with P also being of relevance, but less so than with other contaminants
543 ($r = -0.47$; $p < 0.01$). The ordering of correlation between the different metals and P
544 was also seen in Uchimiya et al.'s study ([2010](#)). The results from both studies showed
545 that P was most important in the precipitation of Pb ($r = -0.59$; $p < 0.01$), followed by
546 Cu ($r = -0.54$; $p < 0.01$) and finally Cd ($r = -0.47$; $p < 0.01$).

547 In contrast to Pb, Cd results indicated that CEC had, at best, a moderate influence on
548 sorption through Ca ($r = 0.34$; $p < 0.01$) and K ($r = 0.40$; $p < 0.01$) with Mg having no
549 discernible correlation with sorption ($r = -0.02$; $p < 0.83$). These findings are in line
550 with other studies where CEC is discounted as a major driver of Cd removal (Mohan et

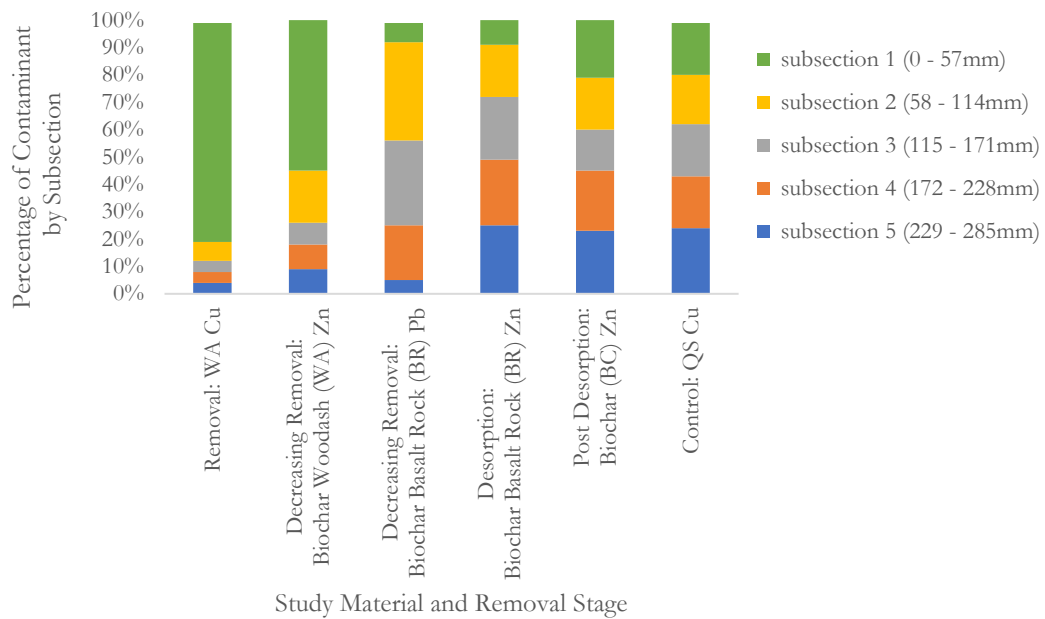
551 al. [2007](#); Uchimiya et al. [2010](#); Xu et al. [2013b](#)). Of all the contaminants studied, Cd is
552 the most toxic and therefore potentially the contaminant of most interest. Other studies
553 have commented on the difficulty of removing Cd and its desorption, in part, due to
554 displacement by Pb (Christophi and Axe [2000](#)). Hence, the success of WA represents a
555 promising pathway to follow.

556 **Feasibility of scaling up**

557 Analysis of the eluate demonstrated the capability of biochar to immobilise heavy
558 metals; analysis of the water column subsections demonstrated the feasibility of scaling
559 this process up. Most prior studies have focused on sorption capacity through
560 laboratory studies, with little to no focus on retention timescales prior to desorption or
561 the consequences on the field management of biochar (Inyang et al. [2012](#); Zhang et al.
562 [2017](#); Schreiter et al. [2018](#)). When analysis of the eluate and the subsections of this
563 study are reviewed together, the potential to scale up deployment of amended biochars
564 as remediators of motorway runoff is apparent. When no desorption is evident through
565 the eluate, such as WA's remediation of Cu (Fig. [4](#)) and there is no indication of
566 desorption, the majority of the contaminant is held in the uppermost subsection
567 (Fig. [11](#)). As sorption capacity is reached, the contaminant travels through the
568 subsections, decreasing the proportions at the higher subsections and increasing
569 proportions in the lower subsections. This can be seen with BR's desorption of Zn (Fig.
570 [6](#)) leading to increasing Zn proportions in the lower subsections (Fig. [11](#)). Post-
571 desorption, as shown by BC's desorption of Zn (Fig. [6](#)), the contaminant has flowed
572 through each subsection leaving the study material and as a result the proportions of
573 contaminant in each subsection are equal in the same way as the control shows equal
574 proportions (Fig. [11](#)). The progression of the contaminant through the study materials
575 indicates that as biochar thickness increases, residence time and the volume of

576 contaminant held increases, thus making scaling up feasible.

577



578

579 **Figure 11.** The progression of heavy metals through biochar. Moving from removal to decreasing
580 removal to desorption then finally to post desorption / control status.

581

582 The retention time of contaminants is key to the viability of using amended biochar in
583 the field due to its intrinsic link with management time and resource. The feasibility of
584 scaling up the use of biochar, alongside its immobilisation properties, provides the
585 opportunity to deploy biochar as a filter for contaminated motorway runoff.

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588

589

Conclusion

590 This work shows that biochar amended with wood ash can be used as an effective
591 remediator of Pb, Cu, Zn and Cd in the field. Its use would combat freshwater
592 degradation contributed to by increased motor vehicle usage and the resultant polluted

593 runoff. In this study, the elimination rates of Pb, Cu, Zn and Cd were shown to differ
594 significantly between biochar (BC), biochar amended with wood ash (WA) and biochar
595 amended with basaltic rock dust (BR). Amended biochar showed significantly more
596 removal of all contaminants (WA > BR > BC). WA was the only study material that
597 did not show signs of desorption in the eluate for any of the contaminants during the
598 36-day study. Pb, Cu, Zn and Cd removal showed strong correlations with pH and total
599 P content indicating that metal speciation, surface charge and precipitation with P were
600 the primary influence on immobilisation. CEC was seen to be relevant in Pb removal,
601 of secondary importance in Cu and Zn removal and of weak or at best moderate
602 importance in Cd removal.

603 In this work, we explored a worst case scenario field situation with pulses and dried
604 columns to approximate issues such as preferential flow and bioavailable metals to
605 maximise toxicity. In these conditions, scaling up the use of biochar to be effective in
606 the field was found to be feasible. Subsection analysis showed that increased thickness
607 of biochar would increase the residence time of the contaminant. Lengthening the
608 efficacy period of the biochar increases the time between removal and replacement of
609 the biochar required in the field, decreasing management time and cost.

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